



Remediation Technologies and Water Treatment Operations

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WISMUT project

- 1946 - 1990, SDAG WISMUT world's no. 4 uranium producer; major foreign uranium supplier to the Soviet Union (~ 216,000 tonnes of U from 20+ deposits)
- 1991, German government new company owner; remediation of one of the most extensive uranium-mining legacies in the world (largest European environmental remediation programme)



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- 7 production complexes, with more than 1,000 objects:
 - 5 underground mines (~ 80 million m³ excavation volume)
 - 1 open pit (~ 84 million m³)
 - 2 processing plants, 10 TMF (160+ million m³ tailings)
 - 60+ waste rock piles (325 million m³ WR)
 - 3,700 hectare operational areas with contaminated facilities

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Wismut remediation activities



- Safe closure of underground mines and controlled mine flooding
- In-situ stabilization or open Pit disposal of mine waste
- Tailings dewatering & stabilization
- Vegetated soil covers on tailings and waste rock
- Dismantling of surface structures, decontamination and site clean-up, disposal of contaminated material into containments
- Environmental monitoring & maintenance
- Water treatment and safe management of residues

Wismut water treatment

- Mine flooding since 1991; water treatment since 1995 (until 2040)
- 4 WTP's for mine drainage, 2 WTP's for TMF seepage and pond water
- Prevailing water treatment technology: modified lime precipitation
- Upcoming technologies: ion exchange, GFH sorption, membrane filtration
- Discharge limits for U, As, $^{226}\text{-Ra}$, heavy metals, Fe, Mn, SO_4 , salt
- Treatment capacity of individual plants 100 - 700 m^3/h (max. 1,200 m^3/h)
- Total throughput ~ 20 million m^3/a
- Total residue volume ~ 25.000 m^3/a , treatment sludge stabilization after dewatering by cement addition (to increase physical and chemical stability)
- Residue deposition on company storage sites



Arsenic retention in lime precipitation plants

- 0.1 – 2 mg/l arsenic in mine and TMF seepage water
- Site specific regulatory limits 10 – 100 µg/l



- aeration ($\sim 5 \text{ m}^3/\text{m}^3$)
- limewater ($\sim 0.05..0.9 \text{ kg}/\text{m}^3$; stepwise, pH $\sim 9-10$)
- KMnO_4 ($\sim 1 \text{ g}/\text{m}^3$)
- BaCl_2 ($\sim 0.1 \text{ kg}/\text{m}^3$)
- FeCl_3 ($\sim 0.1 \text{ kg}/\text{m}^3$)
- flocculation aid
- HDS



- gas exchange, mixing
- oxidation of As, Fe, Mn
- precipitation of iron hydroxide sludge containing As, U, Ra, heavy metals

Ronneburg WTP, 850 m³/h

Arsenic retention in lime precipitation plants

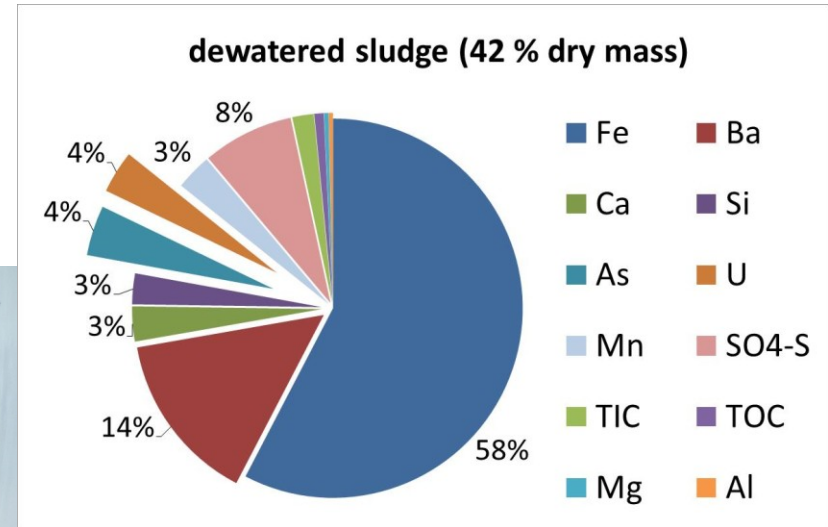
Sludge separation and dewatering

- sedimentation tanks
 - chamber filter presses, centrifuges)
- (30 – 50 wt% solid content)



Sludge stabilization (physical, chemical)

- cement / ash / CaO addition
- (~ 0,5 kg cement / kg sludge)
- crumbly substrates, monolithes

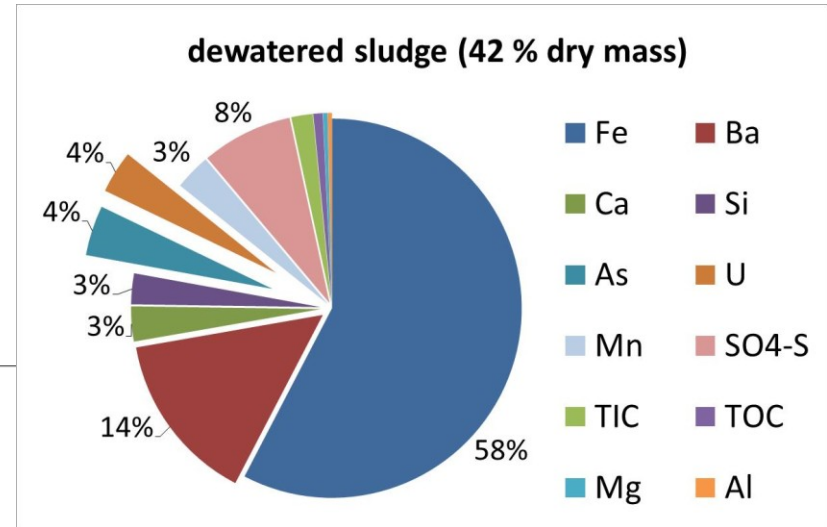
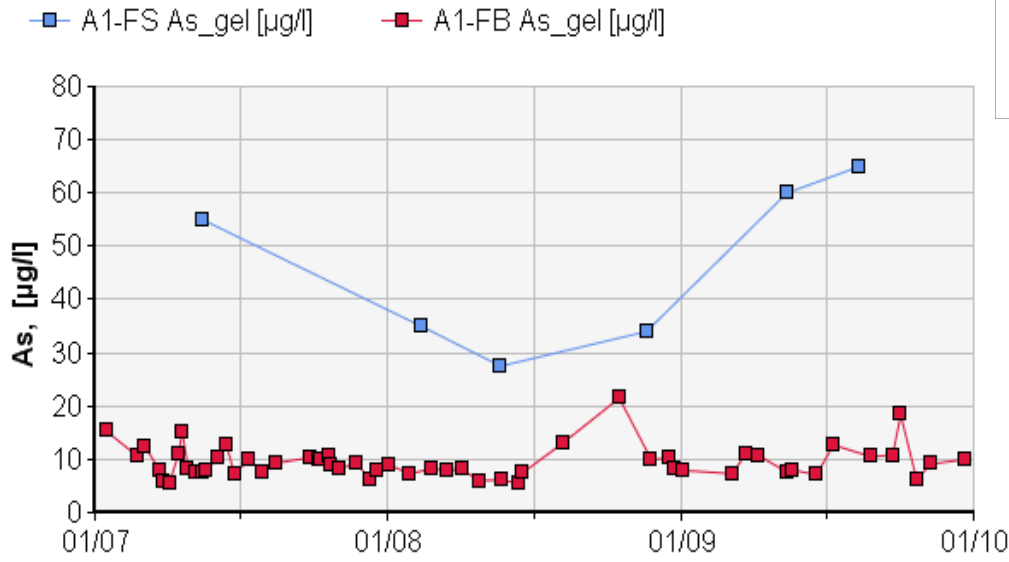


Schlema WTP, 1,200 m³/h

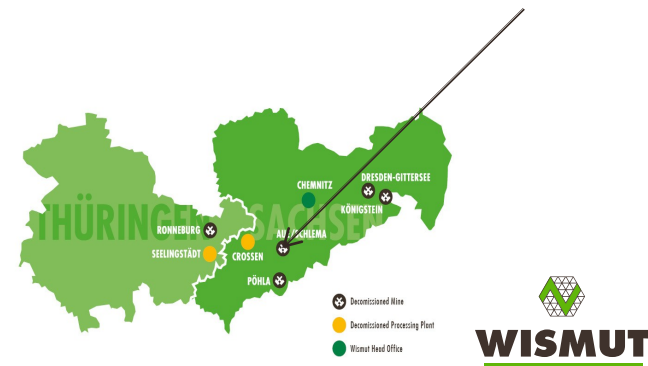


Arsenic retention in lime precipitation plants

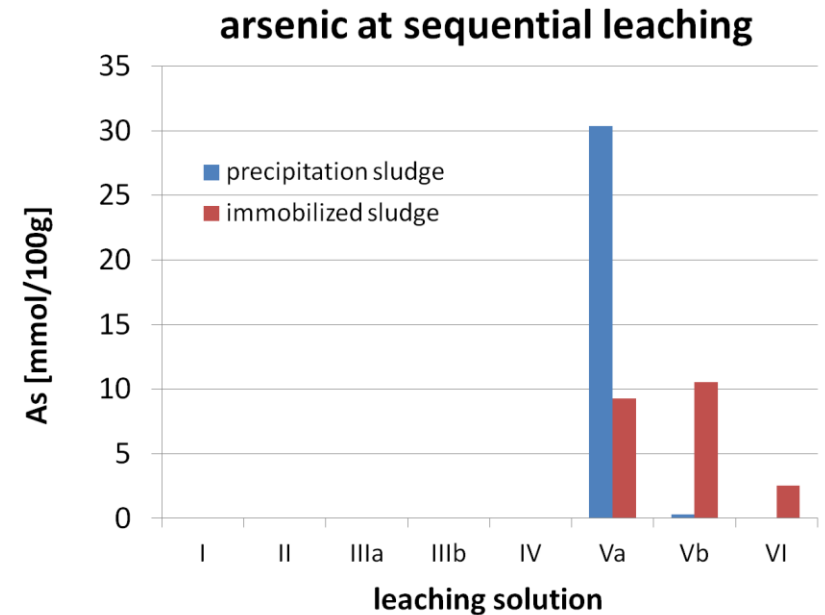
1:10 leaching tests
 blue: dewatered treatment sludge
 red: stabilized treatment sludge



Schlema WTP, 1,200 m³/h



Arsenic retention in lime precipitation



leaching solution	binding form of leached contaminants
I	water soluble form
II	cation exchangeable form
IIIa	carbonates, specific bonds
IIIb	easily reducible minerals
IV	organic complexes
Va	poorly crystalline Fe-oxyhydroxides
V	crystalline Fe-oxides
VI	residual fraction (silicates, sulphides)

Limitations in biochemically reduced mine water

Poehla mine water chemistry

$\text{SO}_4 < 5 \text{ mg/L}$

$\text{U} < 20 \text{ } \mu\text{g/L}$

$\text{pH} = 7 - 7.5$

$E_H = 10 - 100 \text{ mV}$ (CH_4 , H_2)

$\text{Fe} = 5 \text{ mg/L}$ (Ca , Mg , Na , HCO_3)

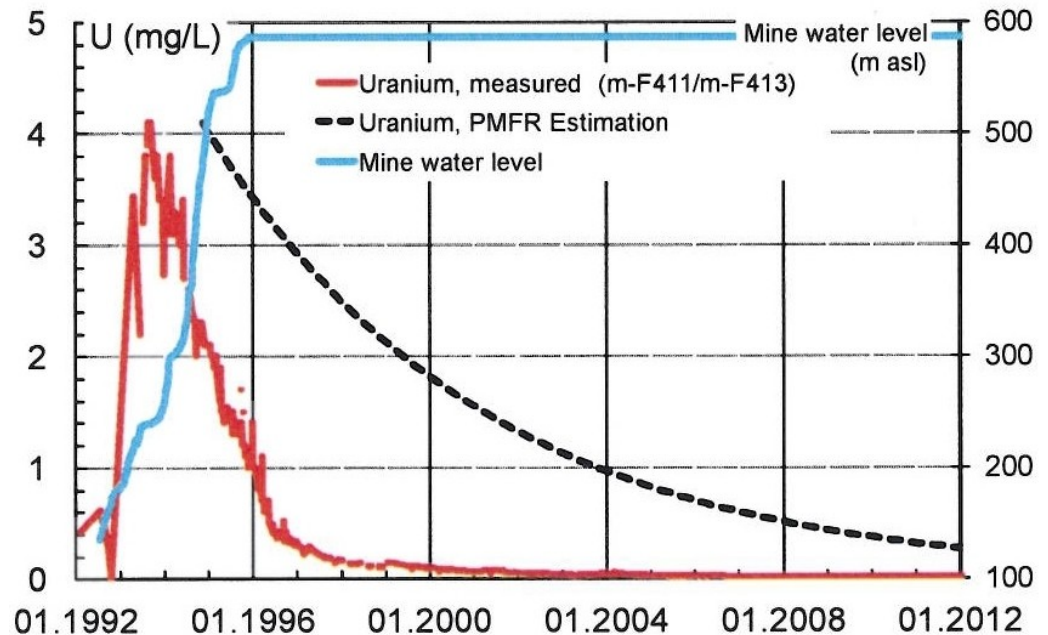
$\text{As} = 2 \text{ mg/L}$

Pohla mine water microbiology

Sulfuricurvum spp., *Sulfurovum* spp.,
Syntrophus spp., *Desulfurivibrio* spp.

Candidatus Methanoperedes,
Methanoregula, *Methanobacterium*

Patinella spp., *Acremonium* spp.



Uranium concentration in mine water Poehla (Paul et al., 2013)



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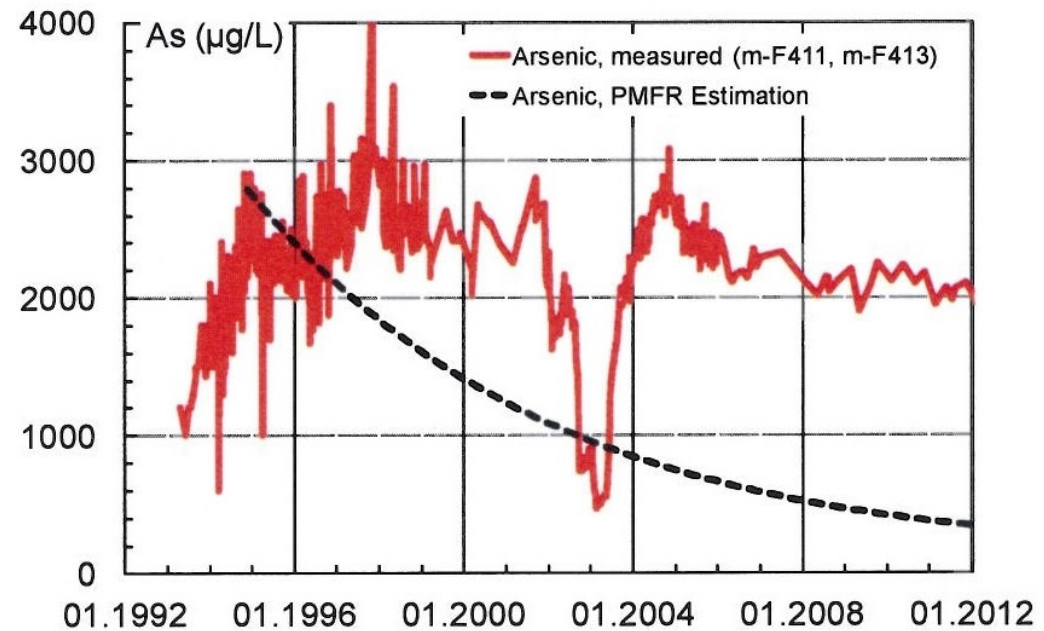
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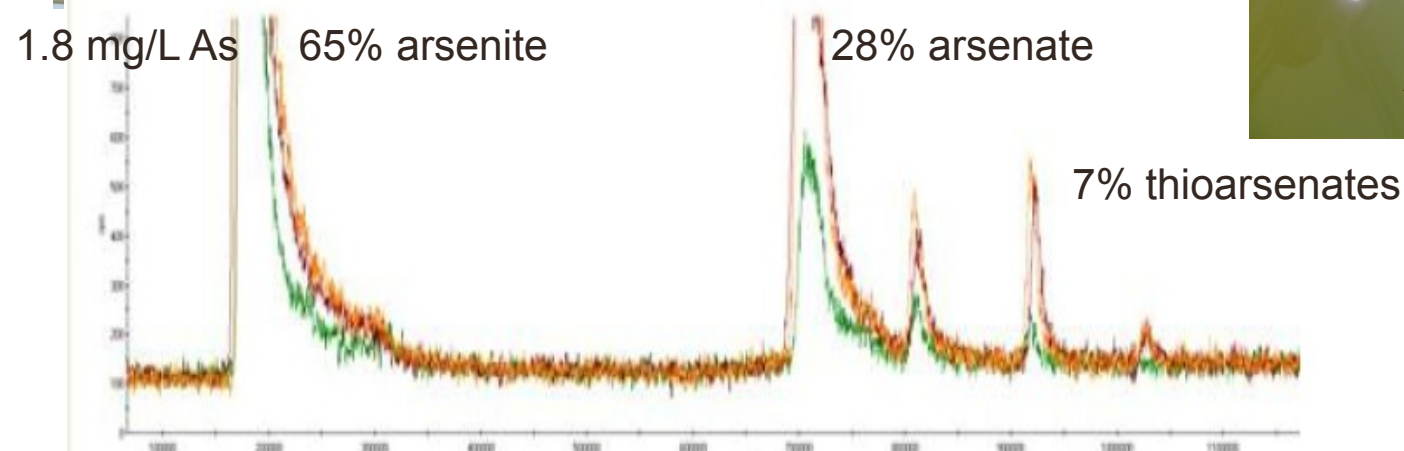
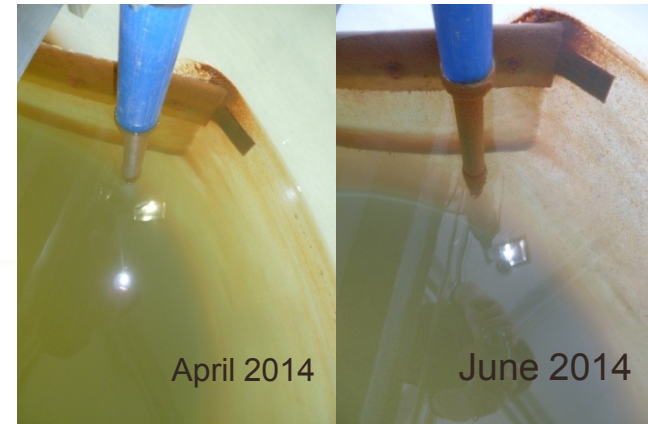
Arsenic concentration in mine water Poehla (Paul et al., 2013)



Limitations in biochemically reduced mine water



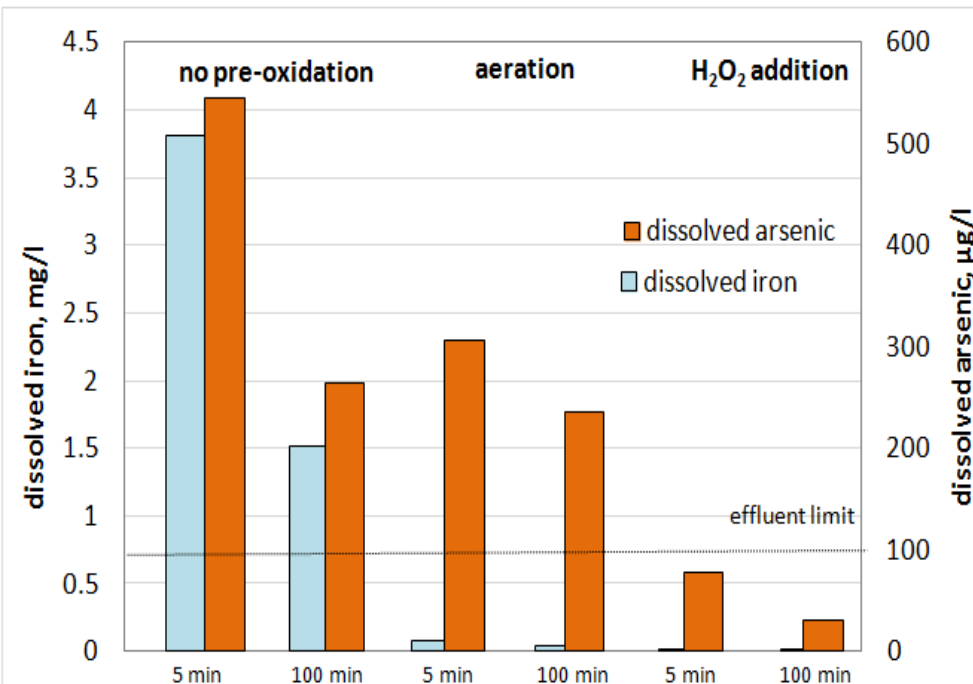
- reduction of ferric iron dosed as precipitation salt
- presence of reduced arsenic species
- hampered flocculation
- poor sludge quality
- insufficient arsenic fixation



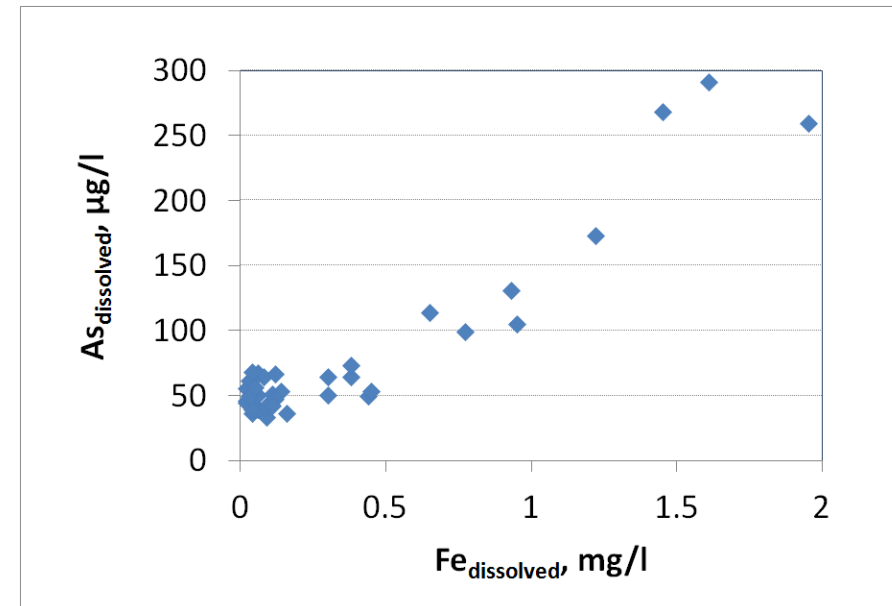
HPLC-GC-MS-Analysis of dissolved arsenic in Poehla mine water (B. Planer-Friedrich, University Bayreuth)

Limitations in biochemically reduced mine water

Lab tests improvement iron flocculation



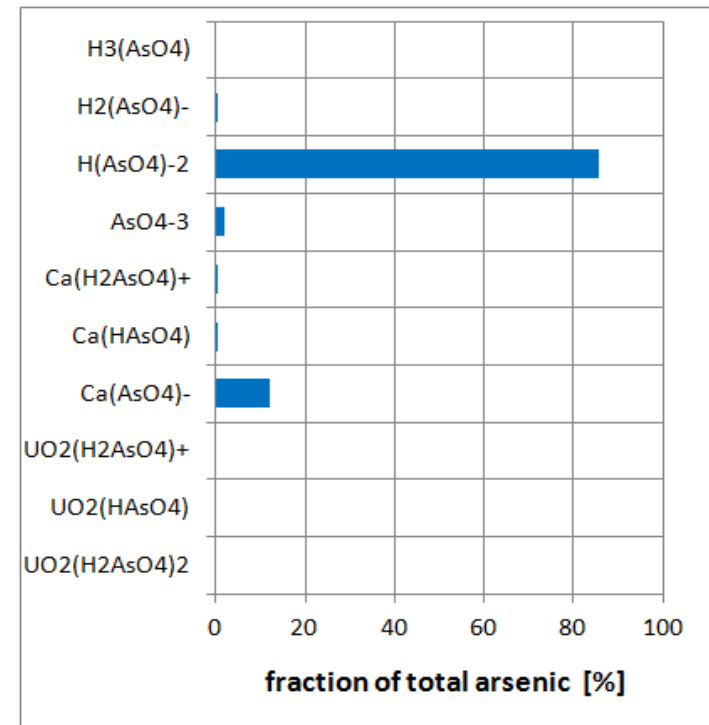
Field results



Arsenic retention by granular ferric hydroxide



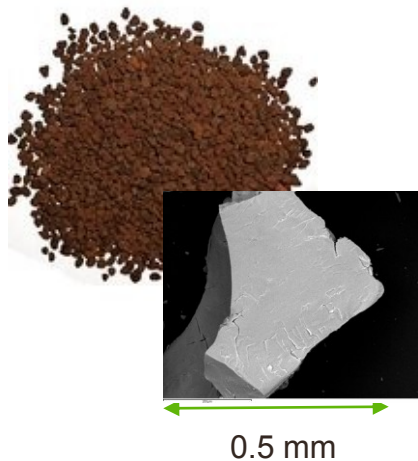
mg/l	pH	U	As	Na	HCO ₃	CO ₃	Cl	SO ₄
10/2014	9.1	4.7	0.5	1,360	1,350	161	419	1,750
03/2015	9.2	7.0	0.6	1,790	1,260	232	509	2,250



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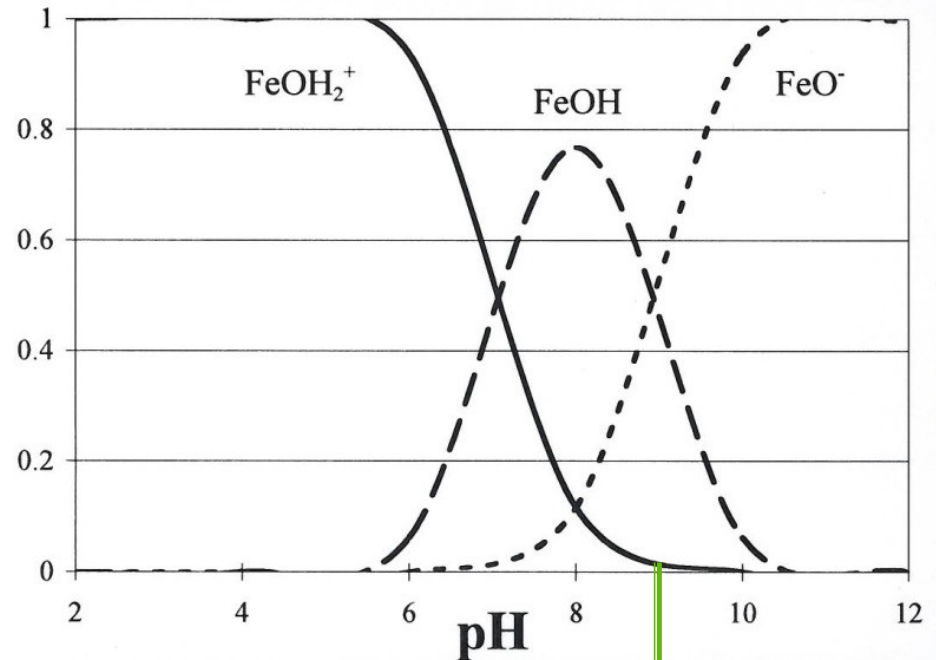
Fixed bed adsorption of arsenic to GFH:

- ferrihydrite adsorption (iron-coprecipitation) BDAT for heavy metal removal from MIW
- GFH adsorption BAT for As removal in drinking water treatment
- waste water application studies for PO_4



FeOH_2^+ , FeOH , FeO^-
(pH depending surface charge, $pzc \sim 7-8$)

Intraparticle
surface diffusion
(sorption kinetics)



$\text{H}(\text{AsO}_4)^{2-}$
 $\text{Ca}(\text{AsO}_4)^-$
pH ~ 9

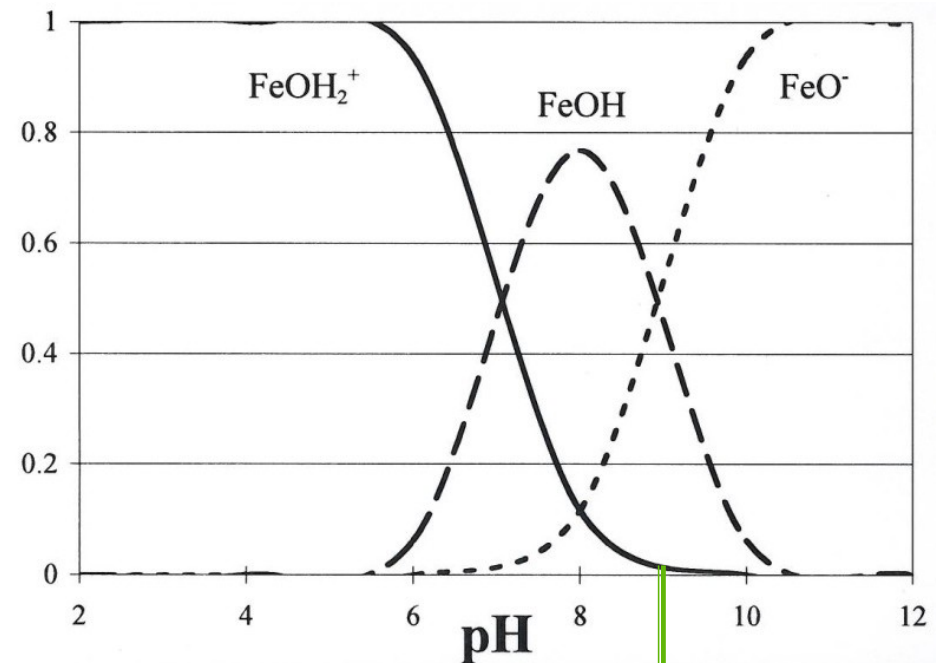
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bed volume 5 ml, GEH,
velocity 10 BV/h, t_r 6 min



←
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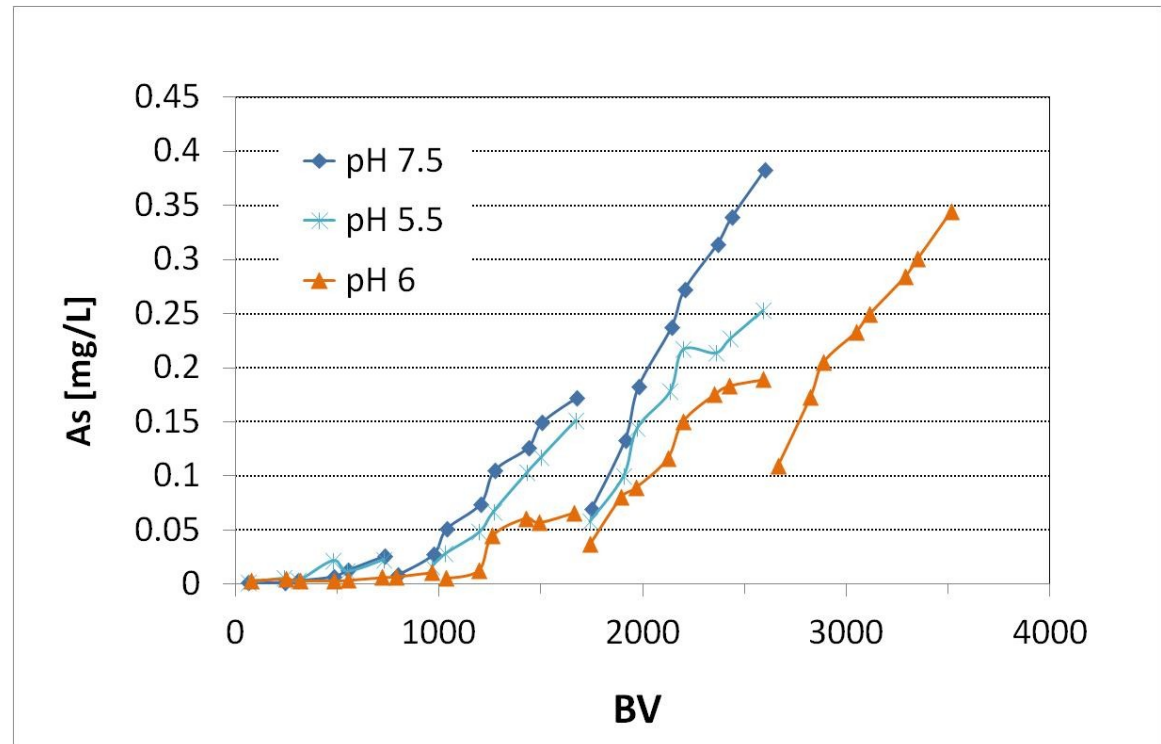
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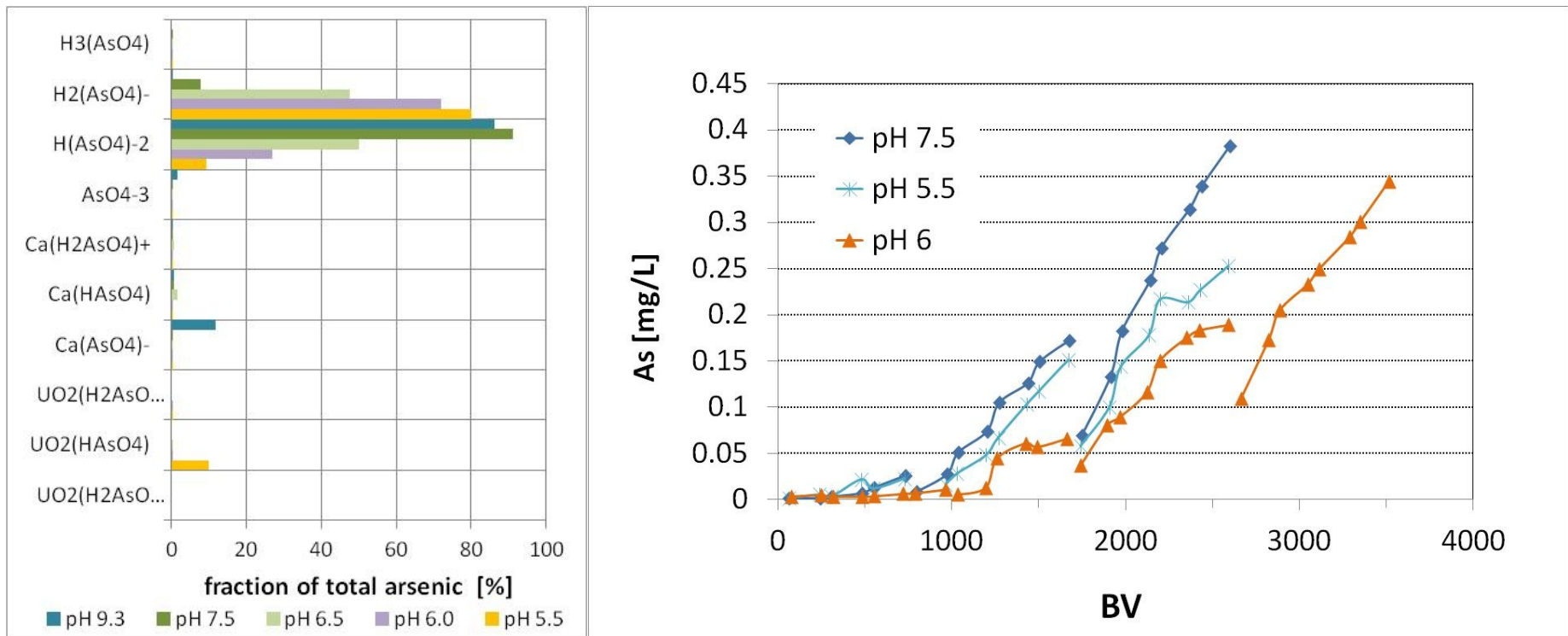
bed volume 5 ml, GEH
(akaganeite, pzc 7.5-8.2),
velocity 10 BV/h, t_r 6 min



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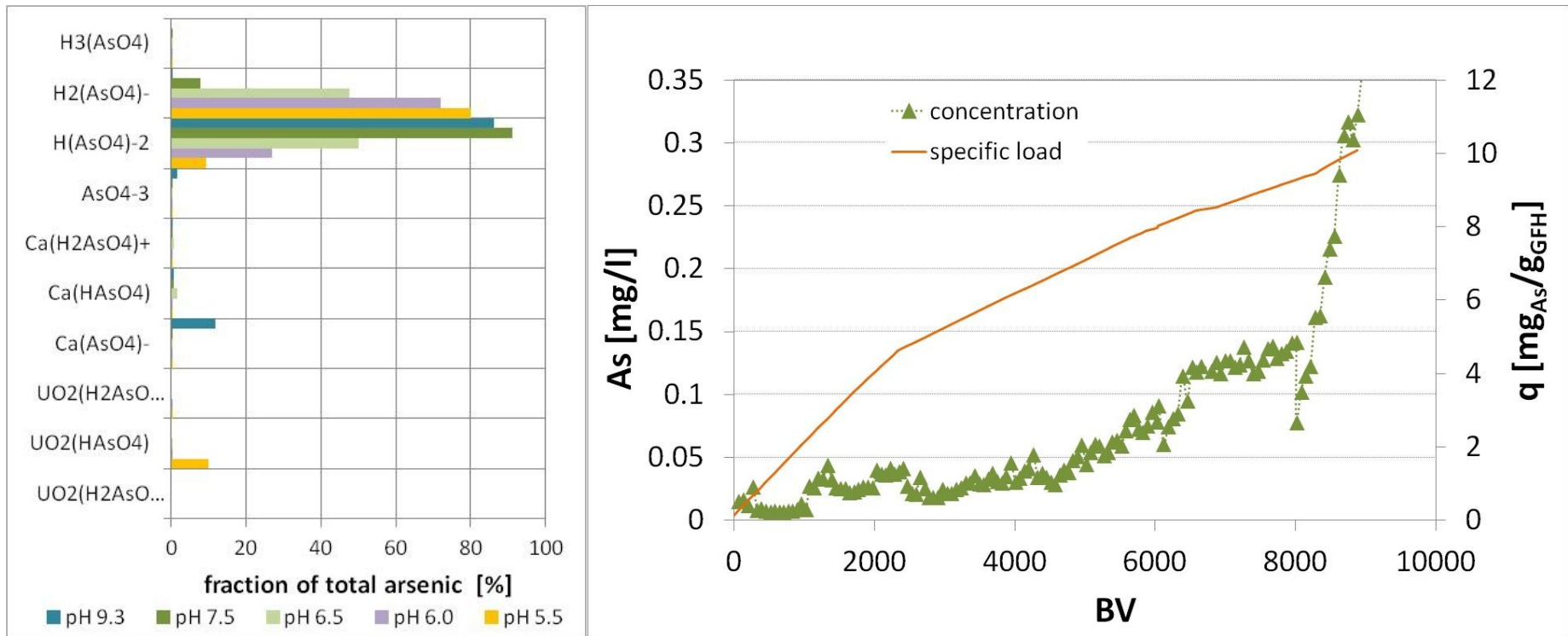


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bed volume 5 ml, FerroSorp (ferrihydrite/calcite, pzc ~ 8), velocity 2.5 BV/h, t_r 24 min, pH 6

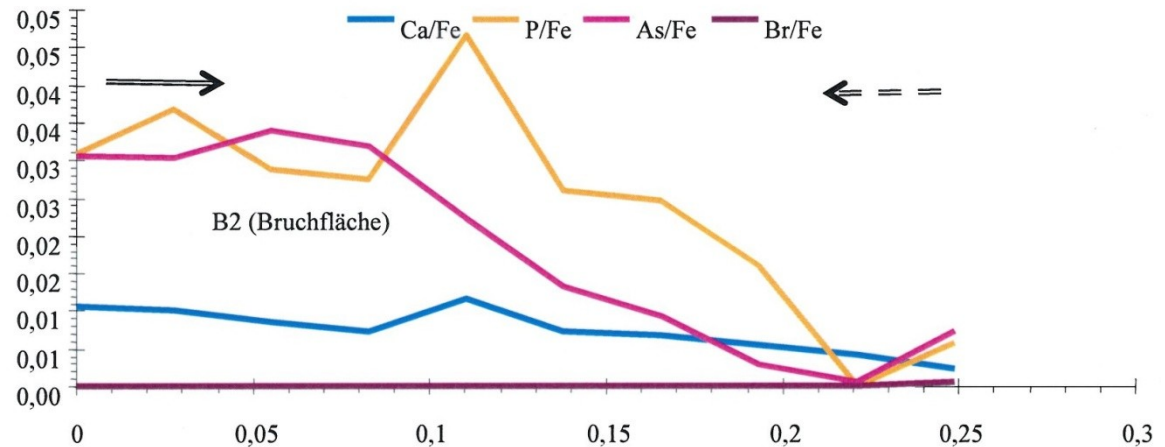
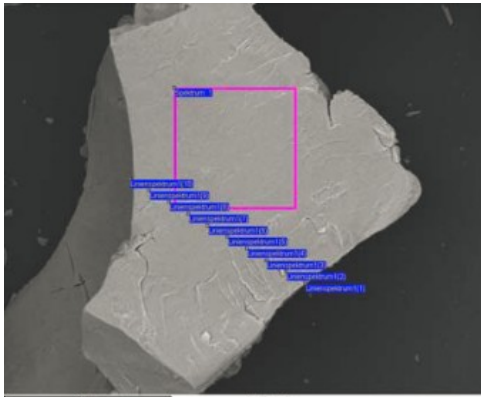
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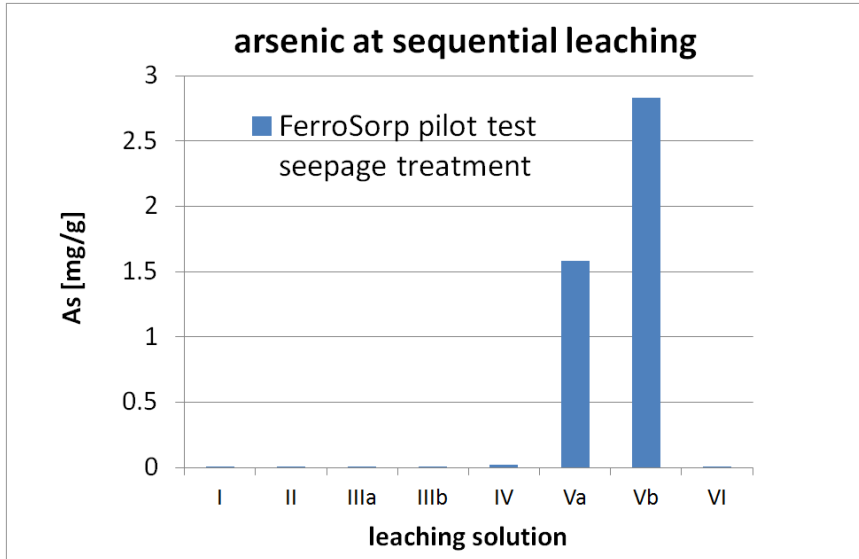
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Results from Lab tests for TMF seepage water treatment:

- pH = 6..6.5 to maximize negative charge of arsenic species and positive charge of HFO surface
- $v = 2.5 \text{ BV / h}$ to allow for intraparticle diffusion
- Specific load: 5 – 10 mg As / g GFH



As - binding stability at GFH



leaching solution	binding form of leached contaminants
I	water soluble form
II	cation exchangeable form
IIIa	carbonates, specific bonds
IIIb	easily reducible minerals
IV	organic complexes
Va	poorly crystalline Fe-oxyhydroxides
V	crystalline Fe-oxides
VI	residual fraction (silicates, sulphides)



1:10 leaching tests (pH-stat: 24 h, pH 4 and 11)

pH		4.0	11.0
EC	mS/cm	2.5	5.17
U	mg/l	0.0191	8.57
As	mg/l	0.009	17.2
K	mg/l	10.6	<25
Na	mg/l	174	1380
Mo	mg/l	<0.02	107
Mg	mg/l	48.5	4.1
Ca	mg/l	174	7.1
Fe	mg/l	<0.02	0.524
SO ₄	mg/l	23	356
CO ₃	mg/l	<5	864
HCO ₃	mg/l	<5	981
TOC	mg/l	0.63	791

Summary WISMUT Arsenic Water Treatment

Lime precipitation plants

- BAT for arsenic removal from MIW
- Sorption and coprecipitation at ferric hydroxides
- Limitations in biochemically reduced mine water – pre-oxidation step required
- Stable As binding in precipitaiton sludge

GFH sorption filter plants

- BAT for arsenic removal from drinking water
- Sorption depends on pH and filter velocity – pH and velocity adjustment required
- Stable As binding at slightly acidic to slightly alkaline pH
- As mobilization at alkaline pH



Thank you for attention!